

**Amendments to the Claims:**

This listing of claims will replace all prior versions and listings of claims in the application:

**Listing of Claims:**

1. (currently amended) A method of stabilizing an olefin metathesis product mixture comprising (a) contacting an olefin metathesis product mixture comprising one or more olefins obtained in a metathesis process, a metathesis catalyst comprising a catalytic metal, optionally, one or more metathesis catalyst degradation products, and optionally, one or more metals derived from sources other than the catalyst and catalyst degradation products, with an adsorbent; or (b) subjecting the olefin metathesis product mixture to a first distillation to remove substantially volatiles and lights, and thereafter, subjecting bottoms from the first distillation to a second distillation in a wiped film evaporator; the (a) adsorbent or (b) distillation method being conducted under conditions sufficient to remove metal(s) to a concentration less than about 30 parts 1 part per million by weight.

2. (currently amended) The method of Claim 1 wherein the olefin metathesis product mixture comprises a C<sub>2-20</sub> substituted or unsubstituted olefin or a mixture thereof, and further, wherein the olefin is a monoolefin or a polyolefin.

3. (canceled) ~~The method of Claim 2 wherein the C<sub>2-20</sub> substituted or unsubstituted olefin is a monoolefin or a polyolefin.~~

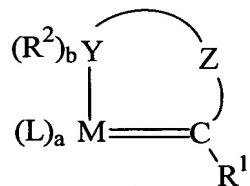
4. (original) The method of Claim 1 wherein the olefin metathesis product mixture comprises a C<sub>2-20</sub> α-olefin, a C<sub>2-20</sub> α,ω-unsaturated acid, a C<sub>2-20</sub> α,ω-unsaturated ester, or a combination thereof.

5. (original) The process of Claim 1 wherein the catalytic metal is selected from ruthenium, tungsten, molybdenum, rhenium, or a combination thereof.

6. (original) The process of Claim 1 wherein the metathesis catalyst is selected from the group consisting of dichloro-3,3-diphenylvinylcarbene-bis(tricyclohexylphosphine)-ruthenium (II), bis(tricyclohexylphosphine)benzylidene ruthenium dichloride, bis(tricyclohexylphosphine)benzylidene ruthenium dibromide, tricyclohexylphosphine[1,3-bis(2,4,6-trimethylphenyl)-4,5-dihydroimidazol-2-ylidene][benzylidene]ruthenium dichloride, tricyclohexylphosphine[1,3-bis(2,4,6-trimethylphenyl)-4,5-dihydroimidazol-2-ylidene][benzylidene]ruthenium dibromide,

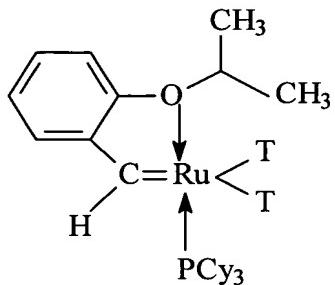
and tricyclohexylphosphine[1,3-bis(2,4,6-trimethylphenyl)-4,5-dihydroimidazol-2-ylidene][benzylidene]ruthenium diiodide.

7. (original) The process of Claim 1 wherein the metathesis catalyst is selected from dichloro-3,3-diphenylvinylcarbene-bis(tricyclohexylphosphine)-ruthenium (II), bis(tricyclohexylphosphine)benzylidene ruthenium dichloride, tricyclohexylphosphine[1,3-bis(2,4,6-trimethylphenyl)-4,5-dihydroimidazol-2-ylidene]{benzylidene}ruthenium (IV) dichloride, tricyclohexylphosphine[1,3-bis(2,4,6-trimethylphenyl)-4,5-dihydroimidazol-2-ylidene]{benzylidene}ruthenium (IV) dibromide, tricyclohexylphosphine[1,3-bis(2,4,6-trimethylphenyl)-4,5-dihydroimidazol-2-ylidene]{benzylidene}ruthenium (IV) diiodide, and chelated ruthenium complexes represented by the following formula:



wherein M is Ru; each L is independently selected from neutral and anionic ligands in any combination that balances the bonding and charge requirements of M; a is an integer, preferably from 1 to about 4, which represents the total number of ligands L; R<sup>1</sup> is selected from hydrogen, straight-chain or branched alkyl, cycloalkyl, aryl, and substituted aryl radicals; Y is an electron donor group of an element from Group 15 or 16 of the Periodic Table; each R<sup>2</sup> is independently selected from hydrogen, alkyl, cycloalkyl, aryl, and substituted aryl radicals sufficient to satisfy the valency of Y; b is an integer, preferably 0 to about 2, representing the total number of R<sup>2</sup> radicals; and Z is an organic diradical that is bonded to both Y and the carbene carbon (C) so as to form a bidentate ligand, which ligand in connection with the M atom forms a ring of from about 4 to about 8 atoms.

8. (original) The process of Claim 1 wherein the metathesis catalyst is:



wherein each T is independently selected from Cl and Br, and PCy<sub>3</sub> is tricyclohexylphosphine.

9. (original) The process of Claim 1 wherein the metathesis catalyst is supported on a catalyst support.

10. (original) The process of Claim 1 wherein metals other than those derived from the catalyst and catalyst degradation products are present and the metals are selected from iron, nickel, copper, zinc, cobalt, chromium, lithium, sodium, potassium, magnesium, calcium, and mixtures thereof.

11. (original) The process of Claim 1 wherein the catalyst degradation product is derived from the reaction of the ligand with oxygen or water.

12. (currently amended) The process of Claim 1 wherein the olefin metathesis product mixture is contacted with an adsorbent selected from carbon, clays, reticular cross-linked ion-exchange resins, alumina, silica-alumina, and mixtures thereof.

13. (canceled) ~~The process of Claim 12 wherein the adsorbent is selected from carbon, clays, reticular cross-linked ion-exchange resins, alumina, silica-alumina, and mixtures thereof.~~

14. (currently amended) The process of ~~Claim 13~~ Claim 12 wherein the adsorbent is a wood carbon.

15. (original) The process of Claim 12 wherein the contacting with adsorbent is effected at a temperature greater than about -5°C and less than about 50°C.

16. (original) The process of Claim 1 wherein the olefin metathesis product mixture is subjected to distillation as in (b) to remove metal(s) to a concentration of less than about 100 ppb.

17. (original) The process of Claim 16 wherein the first distillation to remove lights and volatiles is operated at a temperature greater than about 40°C and less than

about 150°C and a pressure greater than about 15 mm Hg (20 kPa) and less than about 100 mm Hg (132 kPa).

18. (currently amended) The process of Claim 16 wherein the second distillation is conducted in a short path wiped-film evaporator that is operated at a temperature greater than about 150°C and less than about 200°C and at a pressure greater than about 0.001 mm Hg (1.3 Pa) and less than about 5 mm Hg (6.6 kPa).

19. (canceled) ~~The process of Claim 16 wherein the second distillation is conducted in a short path wiped-film evaporator that is operated at a pressure greater than about 0.001 mm Hg (1.3 Pa) and less than about 5 mm Hg (6.6 kPa)~~.

20. (currently amended) The process of Claim 1 wherein the concentration of metal(s) after stabilization is less than about ~~1 ppm~~ 300 parts per billion by weight.

21. (currently amended) A stabilized olefin metathesis product composition comprising one or more olefins produced in a metathesis process and having a total concentration of metals of less than about ~~30 parts 1 part~~ 1 part per million by weight, based on the weight of the olefin metathesis product mixture.

22. (original) The stabilized olefin metathesis product composition of Claim 21 wherein the product olefin is selected from the group consisting of C<sub>2-20</sub> α-olefins, C<sub>2-20</sub> α,ω-unsaturated esters, C<sub>2-20</sub> α,ω-unsaturated acids, and combinations thereof.

23. (original) The composition of Claim 21 further comprising one or more metathesis catalyst ligands, metathesis catalyst degradation products, or a combination thereof.

24. (currently amended) The composition of Claim 21 further comprising a solvent, or a stabilizing ligand, or one or more unconverted reactant olefins, or a mixture thereof.

25. (canceled) ~~The composition of Claim 21 further comprising a stabilizing ligand.~~

26. (canceled) ~~The composition of Claim 21 further comprising one or more unconverted reactant olefins.~~

27. (currently amended) A method of removing metal(s) from an olefin metathesis product mixture comprising contacting a mixture comprising one or more olefins obtained in a metathesis process and one or more catalytic and/or non-catalytic metals with an adsorbent under conditions sufficient to reduce the total metal

concentration to less than about 30 parts 1 part per million by weight, based on the weight of the olefin metathesis product mixture.

28. (original) The method of Claim 27 wherein the adsorbent is selected from the group consisting of carbon, diatomaceous earth, clays, silica gel, reticular cross-linked ion-exchange resins, alumina, silica-alumina, and combinations thereof.

29. (original) The method of Claim 27 wherein the adsorbent is a wood carbon.

30. (currently amended) A method of removing metal(s) from an olefin metathesis product mixture comprising subjecting a product mixture comprising one or more olefins obtained in a metathesis process and one or more catalytic and/or non-catalytic metals to a first distillation under conditions sufficient to remove substantially volatiles and lights, and thereafter, subjecting bottoms from the first distillation to short path wiped-film evaporation under conditions sufficient to reduce the total metal concentration in the olefin product mixture to less than about 30 parts 1 part per million by weight, based on the weight of the olefin metathesis product mixture.

31. (currently amended) The method of Claim 30 wherein the temperature of the short path wiped-film evaporation is greater than about 150°C and less than about 200°C and wherein the pressure in the short path wiped-film evaporator is greater than about 0.001 mm Hg (1.3 Pa) and less than about 5 mm Hg (6.6 kPa).

32. (canceled) The method of Claim 30 wherein the pressure in the short path wiped-film evaporator is greater than about 0.001 mm Hg (1.3 Pa) and less than about 5 mm Hg (6.6 kPa).

33. (currently amended) The method of Claim 27 or 30 Claim 1 wherein the olefin metathesis product mixture comprises 1-decene, methyl decenoate, and methyl oleate.